

This is a sample solution to the project to help in debugging your code.
 Given values are highlighted yellow, calculated values are highlighted orange.

Water for both hot and cold streams

$$T_{h,i} := 360\text{K} \quad T_{h,o} := 300\text{K} \quad T_{c,i} := 278\text{K} \quad T_{c,o} := 283.96\text{K}$$

$$m_h := 0.5 \frac{\text{kg}}{\text{sec}} \quad m_c := 5.0 \frac{\text{kg}}{\text{sec}} \quad U := 100 \frac{\text{J}}{\text{s} \cdot \text{m}^2 \cdot \text{K}} \quad A_c := 29.81 \cdot \text{m}^2$$

$$R_c := \frac{T_{h,i} - T_{h,o}}{T_{c,o} - T_{c,i}} \quad R_c = 10.067$$

$$P_c := \frac{T_{c,o} - T_{c,i}}{T_{h,i} - T_{c,i}} \quad P_c = 0.073$$

$$F_c := \left(\frac{\sqrt{R_c^2 + 1}}{R_c - 1} \right) \cdot \frac{\ln \left(\frac{1 - P_c}{1 - P_c \cdot R_c} \right)}{\ln \left[\frac{2 - P_c \cdot (R_c + 1 - \sqrt{R_c^2 + 1})}{2 - P_c \cdot (R_c + 1 + \sqrt{R_c^2 + 1})} \right]} \quad F_c = 0.965$$

$$\Delta T_1 := T_{h,i} - T_{c,o} \quad \Delta T_1 = 76.04\text{K} \quad \text{Delta T1 for countercurrent heat exchanger}$$

$$\Delta T_2 := T_{h,o} - T_{c,i} \quad \Delta T_2 = 22\text{K} \quad \text{Delta T2 for countercurrent heat exchanger}$$

$$\Delta T_{lm} := \frac{\Delta T_2 - \Delta T_1}{\ln \left(\frac{\Delta T_2}{\Delta T_1} \right)} \quad \Delta T_{lm} = 43.573\text{K} \quad \text{Delta T Log Mean}$$

Heat capacity coefficients from the DIPPR database

$$\begin{pmatrix} A \\ B \\ C \\ D \\ E \end{pmatrix} := \begin{pmatrix} 2.7637E+05 \\ -2.0901E+03 \\ 8.1250E+00 \\ -1.4116E-02 \\ 9.3701E-06 \end{pmatrix} \quad \text{kmol} := 1000 \cdot \text{mol} \quad \text{MW}_{\text{H}_2\text{O}} := 18.01528 \cdot \frac{\text{gm}}{\text{mol}}$$

Molecular weight of water

$$C_p(T) := \left[A + B \cdot \frac{T}{K} + C \cdot \left(\frac{T}{K} \right)^2 + D \cdot \left(\frac{T}{K} \right)^3 + E \cdot \left(\frac{T}{K} \right)^4 \right] \cdot \frac{J}{\text{kmol} \cdot K} \quad \text{Heat capacity}$$

$$c_{p,h} := C_p \left(\frac{T_{h,i} + T_{h,o}}{2} \right) \quad c_{p,h} = 75.285 \frac{J}{\text{mol} \cdot K} \quad \text{Average heat capacity of hot stream fluid}$$

$$c_{p,c} := C_p \left(\frac{T_{c,i} + T_{c,o}}{2} \right) \quad c_{p,c} = 75.825 \frac{J}{\text{mol} \cdot K} \quad \text{Average heat capacity of cold stream fluid}$$

$$q_1 := m_h \cdot \frac{c_{p,h}}{\text{MW}_{\text{H}_2\text{O}}} \cdot (T_{h,i} - T_{h,o}) \quad q_1 = 1.254 \times 10^5 \text{ W} \quad \text{Heat lost from hot stream}$$

$$q_2 := m_c \cdot \frac{c_{p,c}}{\text{MW}_{\text{H}_2\text{O}}} \cdot (T_{h,i} - T_{h,o}) \quad q_2 = 1.254 \times 10^5 \text{ W} \quad \text{Heat gained by cold stream}$$

$$q_3 := F_c \cdot U \cdot A_c \cdot \Delta T_{lm} \quad q_3 = 1.254 \times 10^5 \text{ W} \quad \text{Heat exchanged from hot to cold}$$

All three values for heat transferred are equal, thereby confirming the solution.